Environmental Protection Agency

§ 98.273

(a) Monthly mass of phosphate rock consumed by origin (as listed in Table Z–1 of this subpart) (tons).
(b) Records of all phosphate rock purchases and/or deliveries (if vertically integrated with a mine).
(c) Documentation of the procedures used to ensure the accuracy of monthly phosphate rock consumption by origin, (as listed in Table Z–1 of this subpart).

§ 98.268 Definitions.

All terms used in this subpart have the same meaning given in the Clean Air Act and subpart A of this part.

TABLE Z–1 TO SUBPART Z OF PART 98—DEFAULT CHEMICAL COMPOSITION OF PHOSPHATE ROCK BY ORIGIN

<table>
<thead>
<tr>
<th>Origin</th>
<th>Total carbon (percent by weight)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Central Florida</td>
<td>1.6</td>
</tr>
<tr>
<td>North Florida</td>
<td>1.76</td>
</tr>
<tr>
<td>North Carolina (Calcined)</td>
<td>0.76</td>
</tr>
<tr>
<td>Idaho (Calcined)</td>
<td>0.60</td>
</tr>
<tr>
<td>Morocco</td>
<td>1.56</td>
</tr>
</tbody>
</table>

Subpart AA—Pulp and Paper Manufacturing

§ 98.270 Definition of source category.

(a) The pulp and paper manufacturing source category consists of facilities that produce market pulp (i.e., stand-alone pulp facilities), manufacture pulp and paper (i.e., integrated facilities), produce paper products from purchased pulp, produce secondary fiber from recycled paper, convert paper into paperboard products (e.g., containers), or operate coating and laminating processes.

(b) The emission units for which GHG emissions must be reported are listed in paragraphs (b)(1) through (b)(5) of this section:

1. Chemical recovery furnaces at kraft and soda mills (including recovery furnaces that burn spent pulping liquor produced by both the kraft and semichemical process).
2. Chemical recovery combustion units at sulfite facilities.
3. Chemical recovery combustion units at stand-alone semichemical facilities.
4. Pulp mill lime kilns at kraft and soda facilities.
5. Systems for adding makeup chemicals (CaCO₃, Na₂CO₃) in the chemical recovery areas of chemical pulp mills.

§ 98.271 Reporting threshold.

You must report GHG emissions under this subpart if your facility contains a pulp and paper manufacturing process and the facility meets the requirements of either §98.2(a)(1) or (a)(2).

§ 98.272 GHGs to report.

You must report the emissions listed in paragraphs (a) through (f) of this section:

(a) CO₂, biogenic CO₂, CH₄, and N₂O emissions from each kraft or soda chemical recovery furnace.
(b) CO₂, biogenic CO₂, CH₄, and N₂O emissions from each sulfite chemical recovery combustion unit.
(c) CO₂, biogenic CO₂, CH₄, and N₂O emissions from each stand-alone semichemical chemical recovery combustion unit.
(d) CO₂, biogenic CO₂, CH₄, and N₂O emissions from each kraft or soda pulp mill lime kiln.
(e) CO₂ emissions from addition of makeup chemicals (CaCO₃, Na₂CO₃) in the chemical recovery areas of chemical pulp mills.
(f) CO₂, CH₄, and N₂O combustion emissions from each stationary combustion unit. You must calculate and report these emissions under subpart C of this part (General Stationary Fuel Combustion Sources) by following the requirements of subpart C.

§ 98.273 Calculating GHG emissions.

(a) For each chemical recovery furnace located at a kraft or soda facility, you must determine CO₂, biogenic CO₂, CH₄, and N₂O emissions using the procedures in paragraphs (a)(1) through (a)(3) of this section. CH₄ and N₂O emissions must be calculated as the sum of emissions from combustion of fossil fuels and combustion of biomass in spent liquor solids.

1. Calculate fossil fuel-based CO₂ emissions from direct measurement of fossil fuels consumed and default emissions factors according to the Tier 1 methodology for stationary combustion sources in §98.33(a)(1). A higher
(2) Calculate fossil fuel-based CH₄ and N₂O emissions from direct measurement of fossil fuels consumed, default or site-specific HHV, and default emissions factors and convert to metric tons of CO₂ equivalent according to the methodology for stationary combustion sources in §98.33(c).

(3) Calculate biogenic CO₂ emissions and emissions of CH₄ and N₂O from biomass using measured quantities of spent liquor solids fired, site-specific HHV, and default or site-specific emissions factors, according to Equation AA–1 of this section:

\[
CO_2, \, CH_4, \, or \, N_2O \, from \, biomass = (0.90718) \ast \text{Solids} \ast \text{HHV} \ast \text{EF}
\]  
(Eq. AA-1)

Where:

- CO₂, CH₄, or N₂O, from Biomass = Biogenic CO₂ emissions or emissions of CH₄ or N₂O from spent liquor solids combustion (metric tons per year).
- Solids = Mass of spent liquor solids combusted (short tons per year) determined according to §98.274(b).
- HHV = Annual high heat value of the spent liquor solids (mmBtu per kilogram) determined according to §98.274(b).
- (EF) = Default or site-specific emission factor for CO₂, CH₄, or N₂O, from Table AA–1 of this subpart (kg CO₂, CH₄, or N₂O per mmBtu).
- 0.90718 = Conversion factor from short tons to metric tons.

(b) For each chemical recovery combustion unit located at a sulfite or stand-alone semichemical facility, you must determine CO₂, CH₄, and N₂O emissions using the procedures in paragraphs (b)(1) through (b)(4) of this section:

\[
\text{Biogenic CO}_2 = \frac{44}{12} \ast \text{Solids} \ast \text{CC} \ast (0.90718)
\]  
(Eq. AA-2)

Where:

- Biogenic CO₂ = Annual CO₂ mass emissions for spent liquor solids combustion (metric tons per year).
- Solids = Mass of the spent liquor solids combusted (short tons per year) determined according to §98.274(b).
- CC = Annual carbon content of the spent liquor solids, determined according to §98.274(b) (percent by weight, expressed as a decimal fraction, e.g., 95% = 0.95).
- 44/12 = Ratio of molecular weights, CO₂ to carbon.
- 0.90718 = Conversion from short tons to metric tons.

(4) Calculate CH₄ and N₂O emissions from biomass using Equation AA–1 of this section and the default CH₄ and N₂O emissions factors for kraft facilities in Table AA–1 of this subpart and convert the CH₄ or N₂O emissions to
Environmental Protection Agency § 98.274

metric tons of CO₂ equivalent by multiplying each annual CH₄ and N₂O emissions total by the appropriate global warming potential (GWP) factor from Table A–1 of subpart A of this part.

(c) For each pulp mill lime kiln located at a kraft or soda facility, you must determine CO₂, CH₄, and N₂O emissions using the procedures in paragraphs (c)(1) through (c)(3) of this section:

(1) Calculate CO₂ emissions from fossil fuel from direct measurement of fossil fuels consumed and default HHV and default emissions factors, according to the Tier 1 Calculation Methodology for stationary combustion sources in § 98.33(a)(1). A higher tier from § 98.33(a) may be used to calculate fossil fuel-based CO₂ emissions if the respective monitoring and QA/QC requirements described in § 98.34 are met.

(2) Calculate CH₄ and N₂O emissions from fossil fuel from direct measurement of fossil fuels consumed, default or site-specific HHV, and default emissions factors and convert to metric tons of CO₂ equivalent according to the methodology for stationary combustion sources in § 98.33(c); use the default HHV listed in Table C–1 of subpart C and the default CH₄ and N₂O emissions factors listed in Table AA–2 of this subpart.

(3) Biogenic CO₂ emissions from conversion of CaCO₃ to CaO are included in the biogenic CO₂ estimates calculated for the chemical recovery furnace in paragraph (a)(3) of this section.

(d) For makeup chemical use, you must calculate CO₂ emissions by using direct or indirect measurement of the quantity of chemicals added and ratios of the molecular weights of CO₂ and the makeup chemicals, according to Equation AA–3 of this section:

\[ CO₂ = \left( \frac{M(CaCO₃)}{100} + \frac{M(Na₂CO₃)}{105.99} \right) \times \text{1000 kg/metric ton} \quad \text{(Eq. AA-3)} \]

Where:

\( CO₂ \) = CO₂ mass emissions from makeup chemicals (kilograms/year).

\( M(CaCO₃) \) = Make-up quantity of CaCO₃ used for the reporting year (metric tons per year).

\( M(Na₂CO₃) \) = Make-up quantity of Na₂CO₃ used for the reporting year (metric tons per year).

44 = Molecular weight of CO₂.

100 = Molecular weight of CaCO₃.

105.99 = Molecular weight of Na₂CO₃.


§ 98.274 Monitoring and QA/QC requirements.

(a) Each facility subject to this subpart must quality assure the GHG emissions data according to the applicable requirements in §98.34. All QA/QC data must be available for inspection upon request.

(b) Fuel properties needed to perform the calculations in Equations AA–1 and AA–2 of this subpart must be determined according to paragraphs (b)(1) through (b)(3) of this section.

(1) High heat values of black liquor must be determined no less than annually using T684 om-06 Gross Heating Value of Black Liquor, TAPPI (incorporated by reference, see §98.7). If measurements are performed more frequently than annually, then the high heat value used in Equation AA–1 of this subpart must be based on the average of the representative measurements made during the year.

(2) The annual mass of spent liquor solids must be determined using either of the methods specified in paragraph (b)(2)(i) or (b)(2)(ii) of this section.

(i) Measure the mass of spent liquor solids annually (or more frequently) using T-650 om-06 Solids Content of Black Liquor, TAPPI (incorporated by reference in §98.7). If measurements are performed more frequently than annually, then the mass of spent liquor solids used in Equation AA–1 of this subpart must be based on the average of the representative measurements made during the year.

657