(A) Reduce the emissions in a combustion device to achieve 98 weight percent reduction or to achieve a concentration of 20 parts per million by volume (ppmv) on a dry basis, whichever is less stringent. If an owner or operator elects to comply with the 20 ppmv standard, the concentration shall include a correction to 3 percent oxygen only when supplemental combustion air is used to combust the emissions:

(B) Combust the emissions in a boiler or process heater with a design heat input capacity of 150 million Btu/hr or greater by introducing the emissions into the flame zone of the boiler or process heater; or

(C) Combust the emissions in a flare that complies with the requirements of §63.1333(e).

(2) Limit organic HAP emissions from continuous process vents not included in a material recovery section, as specified in paragraph (c)(1)(i) of this section, by complying with §63.1315.

(3) Batch process vents shall comply with §63.1321.


§ 63.1317 PET and polystyrene affected sources—monitoring provisions.

Continuous process vents using a control or recovery device to comply with §63.1316 shall comply with the applicable monitoring provisions specified for continuous process vents in §63.1315(a), except that references to group determinations (i.e., total resource effectiveness) do not apply and owners or operators are not required to comply with §63.113.

[65 FR 38111, June 19, 2000]

§ 63.1318 PET and polystyrene affected sources—testing and compliance demonstration provisions.

(a) Except as specified in paragraphs (b) through (d) of this section, continuous process vents using a control or recovery device to comply with §63.1316 shall comply with the applicable testing and compliance provisions for continuous process vents specified in §63.1315(a) except that, for purposes of this paragraph (a), references to group determinations (i.e., total resource effectiveness) do not apply and owners or operators are not required to comply with §63.113.

(b) PET affected sources using a dimethyl terephthalate process—Applicability determination procedure. Owners or operators shall calculate emissions from the collection of material recovery sections at an existing affected source producing PET using a continuous dimethyl terephthalate process to determine whether §63.1316(b)(1)(i) is applicable using the procedures specified in either paragraph (b)(1) or (b)(2) of this section.

(1) Use Equation 1 of this subpart to determine mass emissions per mass product as specified in paragraphs (b)(1)(i) and (b)(1)(ii) of this section.

\[
ER = \sum_{i=1}^{n} \frac{E_i}{0.001 P_p}
\]  

where:

- \(ER\) = Emission rate of total organic HAP or TOC, kg/Mg product.
- \(E_i\) = Emission rate of total organic HAP or TOC in continuous process vent \(i\), kg/hr.
- \(P_p\) = The rate of polymer produced, kg/hr.
- \(n\) = Number of continuous process vents in the collection of material recovery sections at the affected source.
- 0.001 = Conversion factor, kg to Mg.

(1) The mass emission rate for each continuous process vent, \(E_i\), shall be determined according to the procedures specified in §63.116(c)(4). The sampling site for determining whether §63.1316(b)(1)(i) is applicable shall be at the outlet of the last recovery or control device. When the provisions of §63.116(c)(4) specify that Method 18, 40 CFR part 60, appendix A shall be used, Method 18 or Method 25A, 40 CFR part 60, appendix A may be used for the purposes of this subpart. The use of Method 25A, 40 CFR part 60, appendix A shall comply with paragraphs (b)(1)(i)(A) and (b)(1)(i)(B) of this section.

(A) The organic HAP used as the calibration gas for Method 25A, 40 CFR part 60, appendix A shall be the single organic HAP representing the largest percent by volume of the emissions.

(B) The use of Method 25A, 40 CFR part 60, appendix A is acceptable if the